

# Understanding Mixing Strategies

for Drug Substance Process  
Development and Scale-Up

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27 June 2018



Vivienne, living with osteoporosis

# Agenda

**Introduction to UCB and work of Chemical Engineers @ UCB**

**Solid-Liquid Separation – Crystallisation development and mixing strategy to develop a robust process**

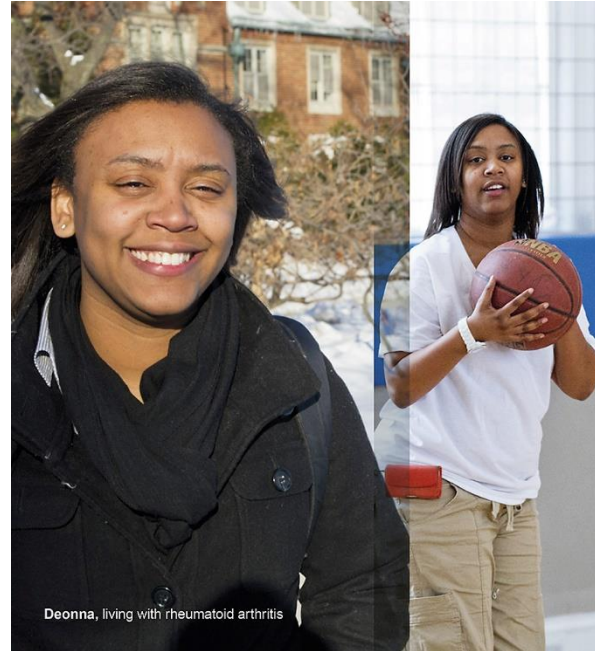
**Final Highlights**

# UCB: creating value for patients

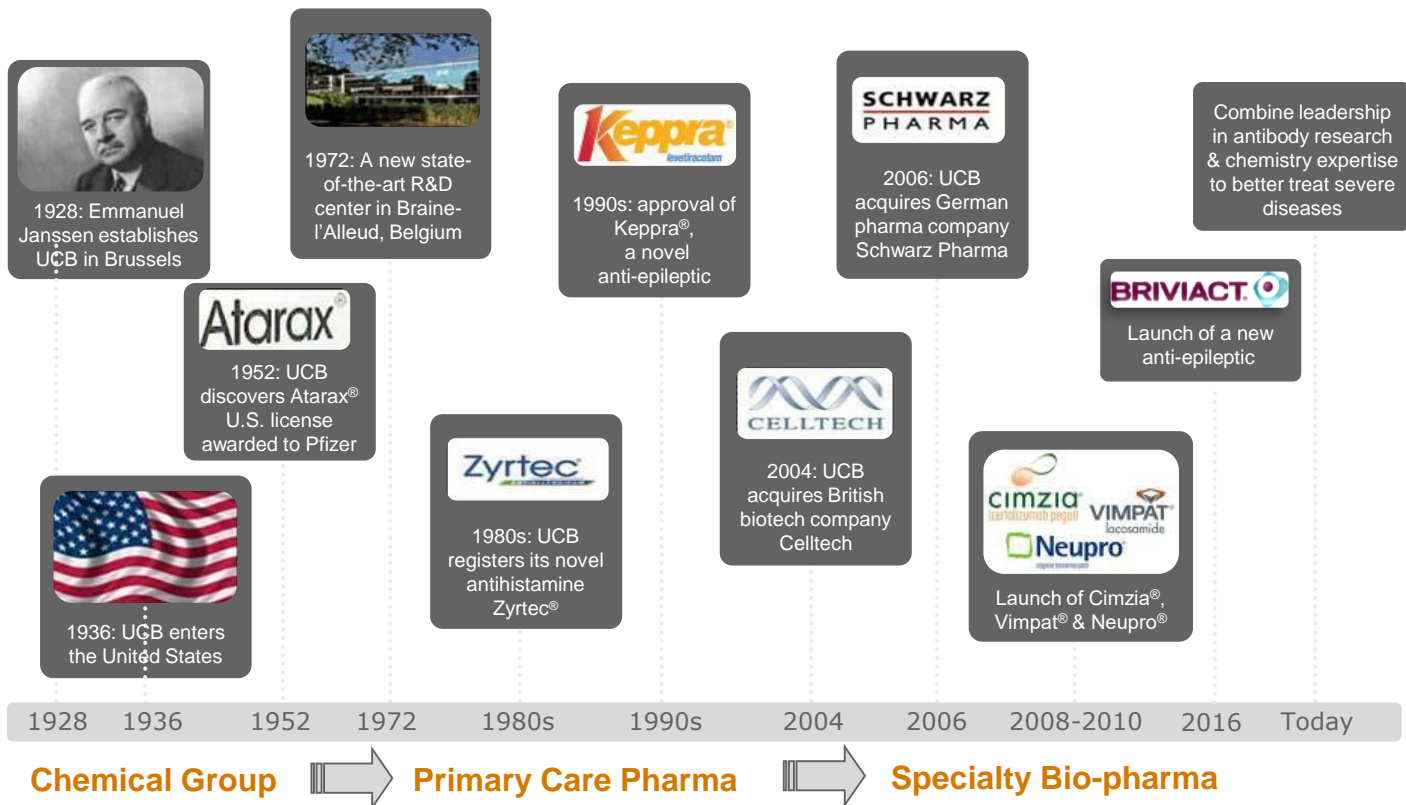
Bringing solutions to people living with *neurological* or *immunological* diseases

## Key facts and figures 2017:

- Revenue: €4.5 billion
- rEBITDA: €1375 million
- About **7500** employees globally
- Operations in **~40** countries
- R&D Spend: **23%** of revenue
- Listed on **Euronext**



# UCB: reinventing itself, leveraging a solid heritage



# Engineering Sciences @ UCB – workflow



**Experiments and  
model predictions  
and verification**



# Solid-Liquid separation: Crystallisation

By Selim Douieb

# Solid-Liquid separation: Crystallisation

Critical unit operation for control of the final product quality

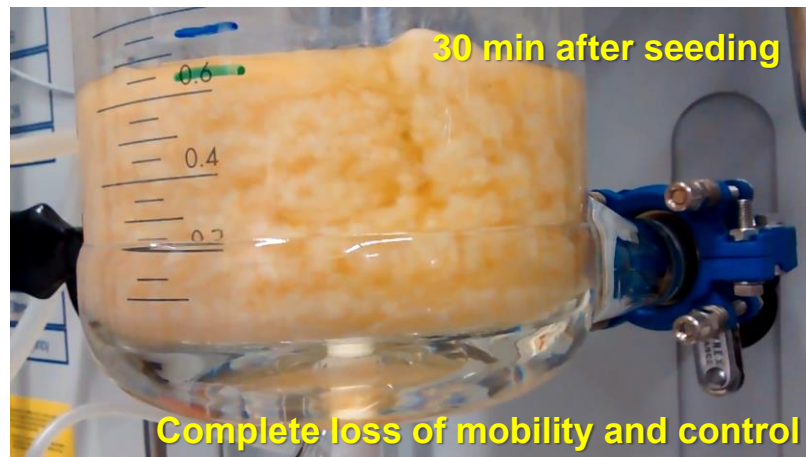
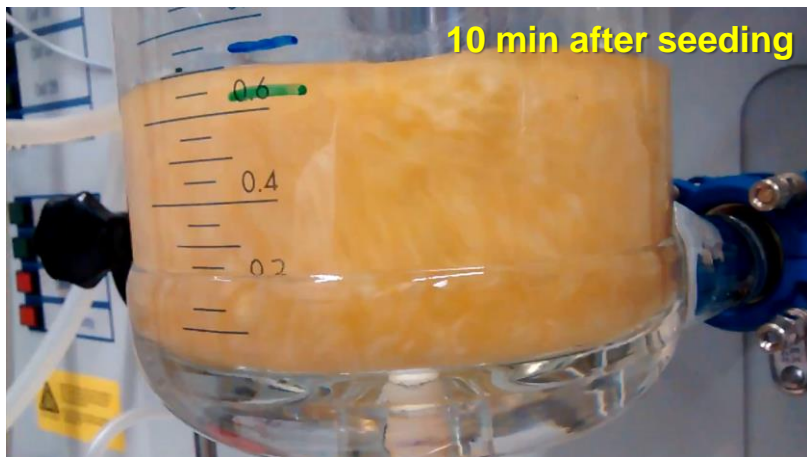
Workhorse of the chemical purification processes to achieve purity, desired form and chemical physical properties of the powder suitable for formulation

To make sure consistency is always delivered at whatever scale the crystallisation is performed, we need to know not only what are the process parameters controlling quality of a process but also understand its physical interactions with equipment = > and this is ever more true for multiphases processes

# Solid-Liquid Separation: Crystallisation

Context: (1) Seeded Antisolvent Addition Cooling Crystallisation

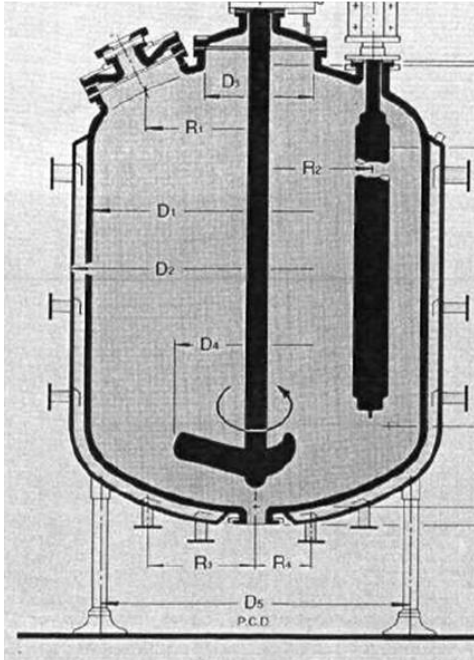
- ❑ Late stage crystallisation development of an highly soluble intermediate;
- ❑ Primary control point for impurities generated by previous RXN steps;
- ❑ Rapid thickening of the suspension upon seeding leading to a complete loss of mobility and control





# Solid-Liquid Separation: Crystallisation

## Context: (2) Development and Scale-up constrains



- ❑ Solvent matrix fixed (Solvent 1/Solvent2), product recovery yield critical (Cost), concentrated solution with low fill level, dilution limited by impact on impurity purging
- ❑ Industrial reactor geometry fixed – thousand glass lined vessel mounting a standard Retreat Curved Impeller (RCI) with single beavertail baffle
- ❑ Impeller rotational speed fixed at high rpm (not variable);
- ❑ Industrial batch size fixed (poor mixing expected due to low fill level and poor baffling);

# Solid-Liquid Separation: Crystallisation

## | Objective

- ❑ Ensure mobility of the crystallisation suspension throughout the entire crystallisation at industrial scale
- ❑ Reproducible yield and crystallisation performance throughout different scales
- ❑ Met target quality – purging of impurities

# Solid-Liquid Separation: Crystallisation

## Methodology

### ❑ Lab scale crystallisation experiments – up to 2L scale

- Process parameters investigated : Dilution – Solvent/antisolvent ratio – Rotational speed (mixing)

### ❑ Mixing characterization and comparison study – up to 30L scale

- Selection of process conditions (Dilution and Solvent/antisolvent ratio) that should ensure a satisfactory mobility of the crystallisation suspension throughout the entire crystallisation at industrial scale

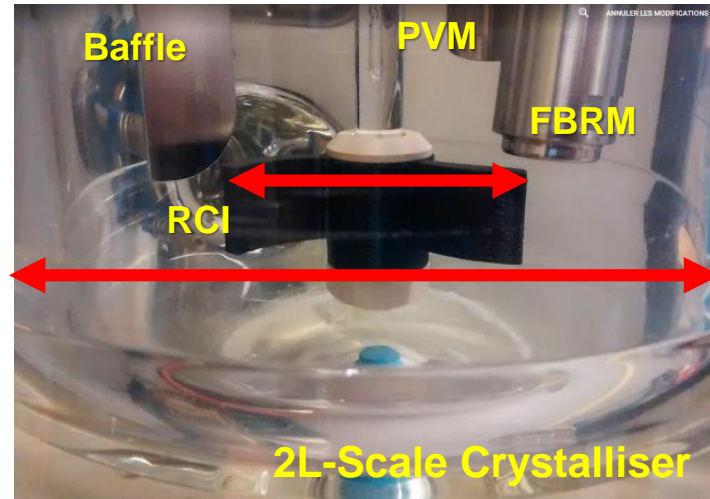
### ❑ Industrial scale validation on a thousand L scale crystallizer

- Process validation on manufactory scale equipment

# Solid-Liquid Separation: Crystallisation

## 2L-scale crystallisation experiments

- ❑ Scale down laboratory 2L vessel mounting a 3 blade retreat curve impeller with torispherical shaped bottom providing good mixing capability
- ❑ Focused Beam Reflectance Measurement (FBRM) and a Particle Vision and Measurement (PVM) probes providing good baffling of the slurry



# Solid-Liquid Separation: Crystallisation

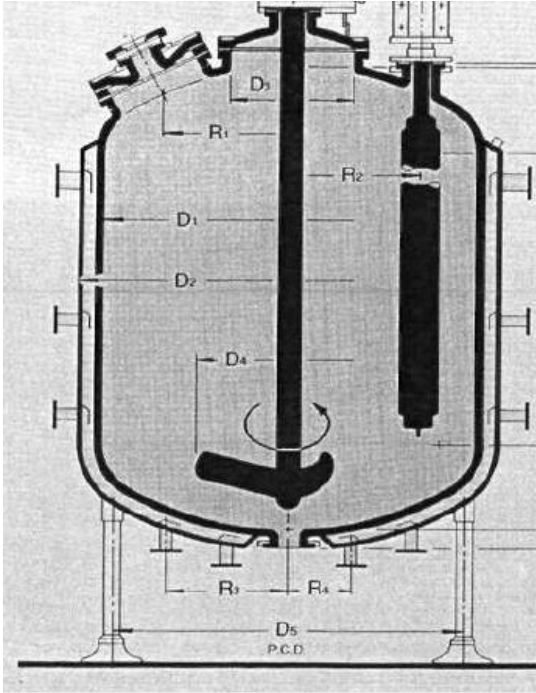
2L-scale crystallisation experiments: results

		→ Total dilution → [v]		
		LOW	MID	HIGH
← $V_{rot}$ ← [rpm]	250	KO	KO	KO
	400	OK	-	-
	600	-	-	OK <sup>*,1</sup>

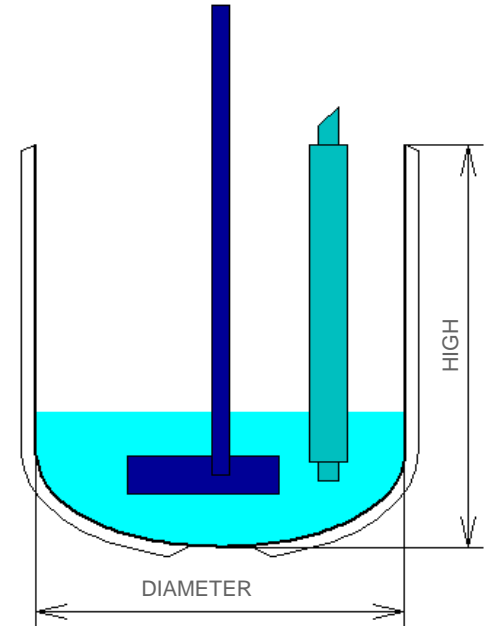
		→ Total dilution → [v]		
		LOW	MID	HIGH
↓ Solvent 1/ Solvent 2 [v/v] ↓	5/4	-	OK	OK
	5/2	OK <sup>*</sup>	OK	-
	5/0	OK	-	-

# Solid-Liquid Separation: Crystallisation

Industrial scale crystallizer – Characterisation by VISIMIX model

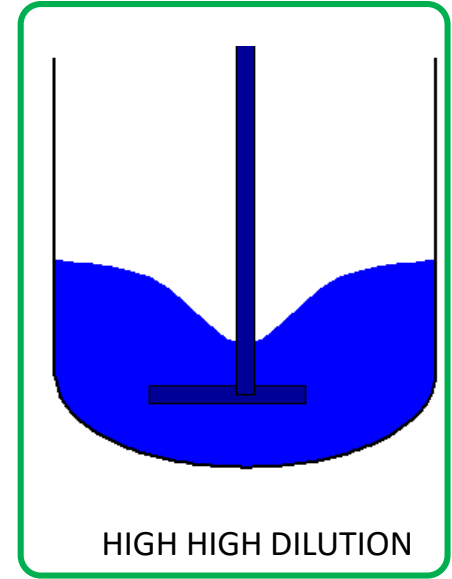
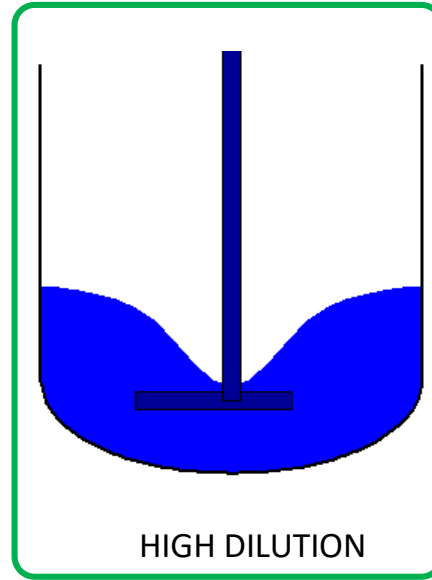
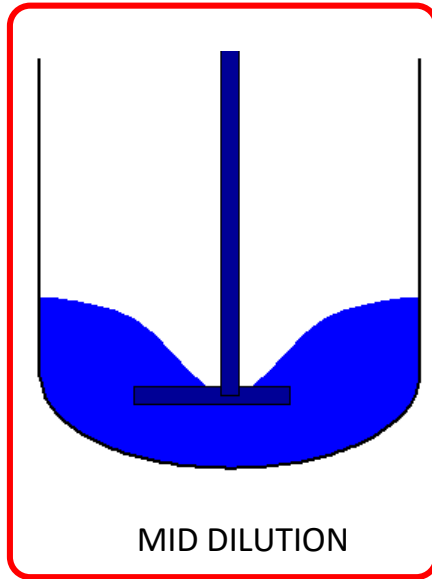
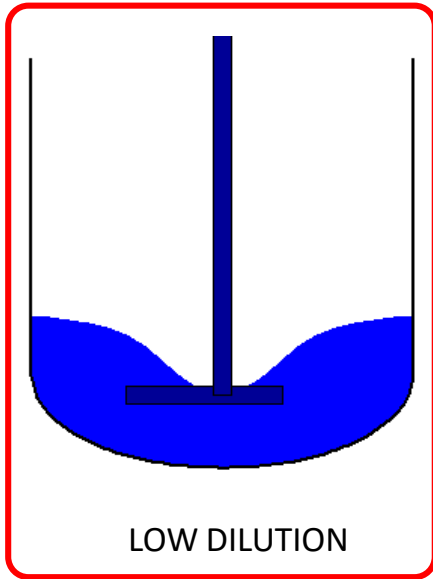


Geometry can  
be directly  
implemented  
in **VISIMIX**



# Solid-Liquid Separation: Crystallisation

Industrial crystalliser – Vortex characterization using VISIMIX



Vortex touches impeller: shaft vibration and gas entraining from surface are potential issue

Minimum fill level required to avoid vortex  
high reaching impeller

# Solid-Liquid Separation: Crystallisation

## | 2L-scale crystallisation experiments: results

- ❑ For the **seeded cooling crystallisation** in solvent 1 only a certain mixing intensity threshold was required to maintain mobility and control throughout;
- ❑ For the **seeded antisolvent addition cooling crystallisation** higher total dilutions did also prevent mobility losses after seeding at critical mixing intensity.



# Solid-Liquid Separation: Crystallisation

## Mixing characterization and comparison study – VISIMIX

- ❑ **For a solid-free crystallisation solution VISIMIX allowed the calculation of two critical mixing parameters:**
  - The average specific power input,  $\bar{\epsilon}$  [W/kg]
  - The turbulent shear rate at impeller tip,  $\dot{\gamma}_{tip}$  [s<sup>-1</sup>]
- ❑ **What are the relevant scale-up parameters?**
- ❑ **How the mixing used so far on small scale equipment will compare with what is achievable at manufactory scale?**
- ❑ **Mixing calculations were relatively straight forward with VISIMIX for the manufactory equipment but what about the laboratory equipment?**

# Solid-Liquid Separation: Crystallisation

## Laboratory scale equipment – building VISIMIX model

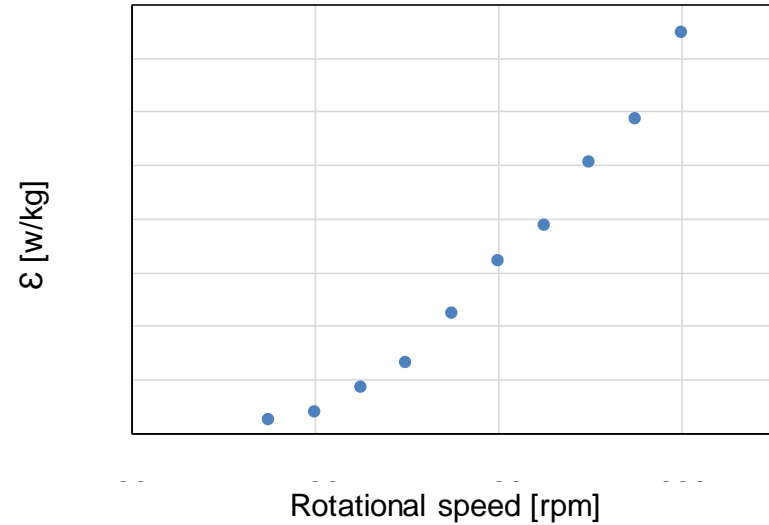
- **Need to select an appropriate model for the laboratory equipment in VISIMIX to evaluate the scale-up on manufactory scale;**
  - STEP 1 - Experimental characterization of the effect of  $V_{rot}$  on  $\varepsilon$  (for a given volume of liquid) in the 2L vessel;
  - STEP 2 – Generate several Visimix models of the 2L reactor with different realistic baffle arrangements;
  - STEP 3 - Select the model enabling to reproduce the experimental characterization results with the highest accuracy.

# Solid-Liquid Separation: Crystallisation

Laboratory scale equipment – measurements



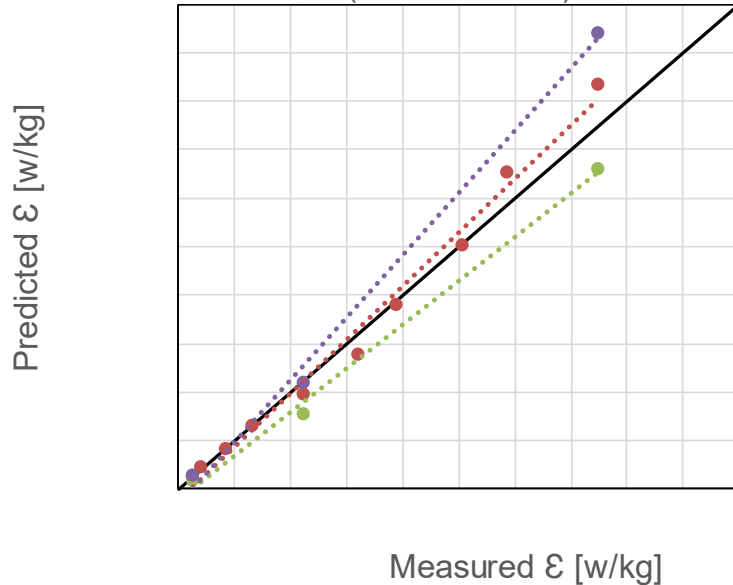
Measured  $\epsilon$   
(1L Solvent 1)



# Solid-Liquid Separation: Crystallisation

## Laboratory scale equipment – comparison

Measured vs. Predicted  $\varepsilon$   
(1L Solvent 1)



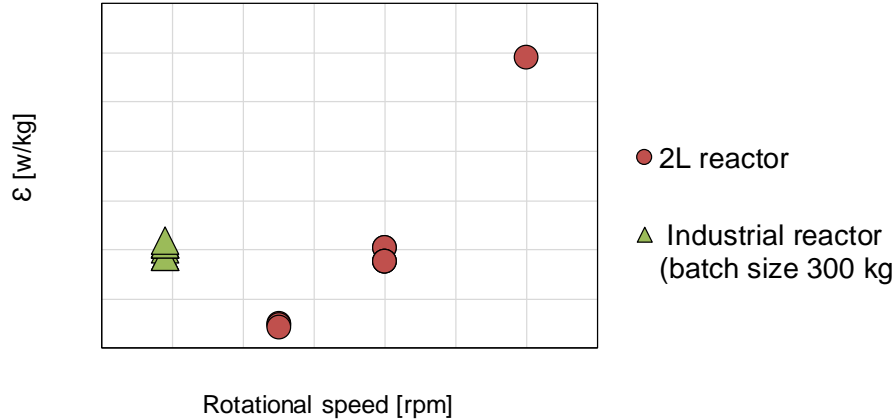
	Baffling configuration 1	Baffling configuration 2	Baffling configuration 3
Baffle type	Beavertail	Beavertail	Beavertail
number	2	1	3
width [mm]	15	15	15
dist. From bottom	40	40	40
dist. From wall [mm]	14	14	14

Satisfactory  
baffle configuration

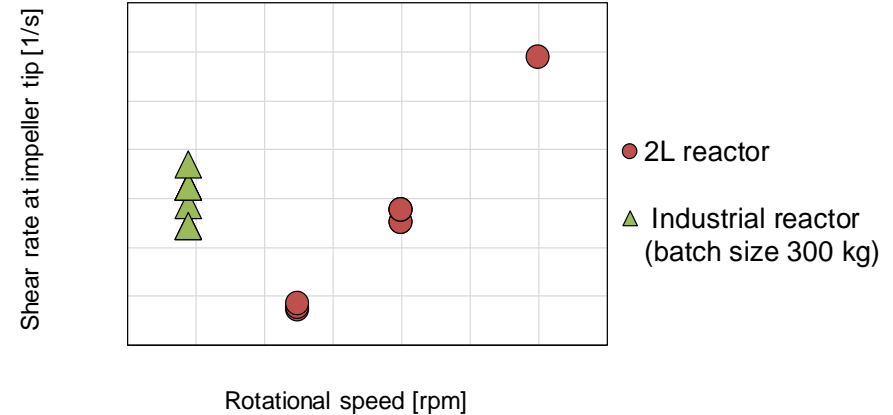
# Solid-Liquid Separation: Crystallisation

## SCALE-UP calculations and comparison - VISIMIX

Predicted  $\epsilon$  for the investigated experimental conditions



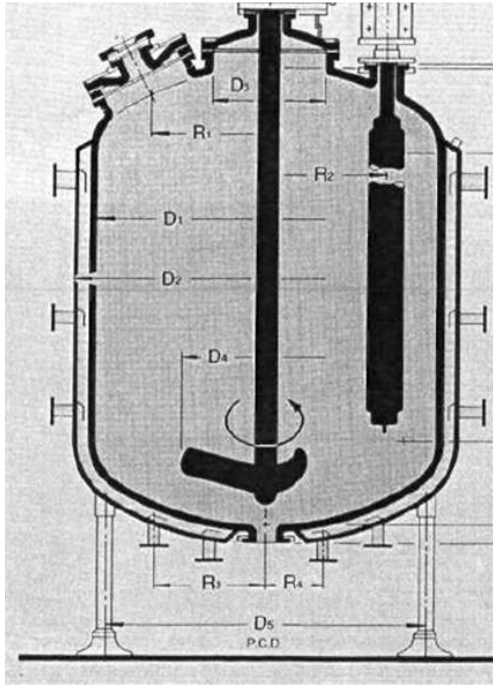
Predicted shear rate at impeller tip for the investigated experimental conditions



**Process conditions leading to a satisfactory mobility/control of the crystallisation throughout the entire crystallisation process @ 2L-scale for a given rotational speed are expected to also give satisfactory results in the industrial scale crystallizer**

# Solid-Liquid Separation: Crystallisation

Industrial scale validation – thousand L scale crystallizer



- ❑ Dilution HIGH - Solvent/antisolvent ratio HIGH
- ❑ @ batch size of hundreds of kg
- ❑ Good mobility at all time
- ❑ Vortex did not touch impeller →
- ❑ Form, yield and purgibility of imps met



# Understanding Mixing Strategies

## | Highlights

- ❑ **Reliable mixing models are critical support tools for the process engineer in the pharmaceutical industry**
- ❑ **Reliable scale-up is not any longer about appropriate process conditions only but it is about understanding how process interacts with the physical environment – ultimately this will lead to more process flexibility and less chance of failure – to more efficient and economic processes**

# Questions?



# Thanks!